

OPTIMIZATION OF AQUEOUS-BASED FILM COATING PROCESS PARAMETERS CONTAINING GLUCOSAMINE SULFATE POTASSIUM CHLORIDE

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ABSTRACT

Objective: The aim of the present work was to prepare film-coated tablet of glucosamine sulfate potassium chloride and study the effect of coating process parameters which implicate more significant effects on an aqueous-based film coating process of tablets.

Methods: The different batches of uncoated tablets were prepared by wet granulation method. Aqueous film coating was carried out by using opadry®II white 85F18422. A 3² full factorial design was employed to study the effect of spray rate (X₁) and inlet air temperature (X₂) on coating uniformity, coating process efficiency and % loss on drying. The surface characteristics of the aqueous-based film-coated tablet were studied using a SEM. Check point batch was prepared to validate the evolved model.

Results: Preliminary trials indicated that individual process parameters affected the quality of coated tablets. Hence, studied the combined effect of these factors on the coating process required and 3² full factorial design was applied. In this study, it was seen that the spray rate and inlet air temperature had a major effect on tablet coating process. It was observed from factorial batch that maximum drug release was found in batch F5.

Conclusion: The results of full factorial design indicate both parameters spray rate (X₁) and inlet air temperature (X₂) have a significant effect on coating process and batch F5 is stable for 3 mo at the accelerated condition.

Keywords: Glucosamine sulfate potassium chloride, 3² full factorial design, Aqueous-based film, Spray rate, Inlet air temperature

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INTRODUCTION

Glucosamine sulfate potassium chloride (GS-K) is a naturally occurring chemical found in the human body. It resides in human cartilage connective tissue that serves as a joint cushion in the knees, hips and joints [1, 2]. It is used in the treatment of osteoarthritis. GS-K is highly hygroscopic and degrades rapidly when exposed to moisture or air. So it's creating problems in shelf-life and bioavailability [3, 4].

Oral route of drug administration is the most appealing route for drug delivery. Among the oral dosage form tablet are most preferred dosage forms because of its ease to manufacturing, convenience in administration and accurate dosing. Film coating and sugar coating of the tablets is an additional step in the manufacturing process which increases the cost of products [5, 6]. Film coating is carried out by using organic solvent or aqueous coating. Aqueous coating of oral solid dosage forms has rapidly replaced solvent-based coating for safety, environmental and economic reasons. In, aqueous coating processing parameters like spray rate, inlet air temperature, pan speed, atomizing air pressure are important issues [7, 8].

GS-K of orally administered drugs exhibit moisture sensitive characteristics that create stability problem in the aqueous coating. The slower rate of evaporation gives rise to the possibility of water penetrating; this could result in either physical degradation of the drug. So, the present work was carried out by optimizing various processing parameters and improves the stability and shelf-life of the product.

MATERIALS AND METHODS

Materials and reagents

Glucosamine sulfate potassium chloride was received as a generous gift from Jenburkt Pharmaceuticals Ltd. Sihor, Gujarat, India. Opadry II 85F18422 white was obtained from Colorcon, Goa, India. Microcrystalline cellulose (PH 101) and Microcrystalline cellulose (PH 102) were purchased from SAVA Fine Chemical, Mumbai, Maharashtra, India. All other materials and chemicals used were of either pharmaceutical or analytical grade.

Drug excipients compatibility study

The physicochemical compatibilities of drug and excipients were tested by differential scanning calorimetric (DSC) analysis. DSC thermograms of the drug and drug-excipients physical mixtures (1:1 wt/wt) were derived from a DSC with a thermal analysis performed by using an automatic thermal analyzer system (DSC 60, Shimadzu, Japan). The analysis was performed at a rate of 10 °C/min from 50 °C to 250 °C under a nitrogen flow of 20 ml/min [9, 10].

Development of glucosamine sulfate potassium chloride core tablet

The tablets were formulated by wet granulation technique and the whole process like dispensing; sifting, milling and compression were done under the controlled temperature and humidity. All the ingredients were individually screened through sieve no. 60, except glidants and lubricant. Povidone K30 and methylparaben were dissolved in isopropyl alcohol (IPA) which was used as a binder. Dibasic calcium phosphate and microcrystalline cellulose (Avicel PH 101) was used as diluents. Granulation was carried out in two-liter capacity rapid mixing granulator (RMG) and drying was carried out in fluid bed dryer (FBD) until LOD was dropped below 2 %. Compression was carried out using 16 station "D" types tooling rotary compression machine. Composition of core formulation described in table 1 [12, 13].

Preliminary screening of coating parameters

GS-K core tablet were coated by using 10% suspension of opadry® II 85F18422 white in water. Core tablets were loaded into pre-warmed coating pan. Then spray of the coating dispersion was started along with the regulation of various coating parameters like atomizing air pressure (1.8 Bar), pan speed (9-11 rpm), spray rate and inlet air temperature as described in table 3. Spraying process was continued until about 3% weight gain was achieved on the core tablets. Then the coated tablets were dried for 15 min at about 50 °C of inlet air temperature [14, 15].

Evaluation parameters of glucosamine sulfate potassium chloride core tablet

Thickness, Hardness, Weight variation, Drug content uniformity, % Friability and Disintegration test of the formulations were measured

as described by Yadav K et. al, Khar RK et. al, Madgulkar AR et. al,

and Lakade SH et. al, respectively [16-19].

Table 1: Formulation of glucosamine sulfate potassium chloride core tablet

Batch No.	T1	T2	T3	T4	T5
Ingredients	Quantity (mg/tablet)				
Glucosamine sulfate potassium chloride	750	750	750	750	750
Microcrystalline cellulose (Avicel PH 101)	187.5	177.5	172.5	162.5	152.5
Dibasic calcium phosphate (Anhydrous)	100	100	100	100	100
Methyl paraben	0.5	0.5	0.5	0.5	0.5
Povidone K30	20	30	35	35	35
Isopropyl alcohol	Q. S.	Q. S.	Q. S.	Q. S.	Q. S.
Sodium starch glycolate	10	10	10	20	30
Microcrystalline cellulose (Avicel PH 102)	25	25	25	25	25
Magnesium stearate	7	7	7	7	7
TOTAL	1100	1100	1100	1100	1100

Evaluation of coating parameters

Coating uniformity

The Coating uniformity was measured as the variation in weight gain of coated tablets. The reported standard deviation (SD) was calculated as:

$$SD = \left\{ \frac{\sum[(wt_{ai} - wt_{bi}) - x]^2}{n-1} \right\}^{\frac{1}{2}}$$

Where, wt_{ai} and wt_{bi} are the weights of tablet i after and before coating, respectively, n is the number of tablets measured and x is the average weight gain of the n measured tablets from coating [20, 21].

% Coating process efficiency

The % Coating process efficiency (% CPE) will be measured as the actual percent weight gain relative to the theoretical percent. Coating process efficiency was determined by the following equation:

$$CPE = \frac{\% wga}{\% wgt} \times 100$$

Where, wgt is the theoretical percent weight gain and wga is the actual percent weight gain, before and after coating, respectively [22, 23].

% Loss on drying

The % loss on drying (% LOD) is the moisture content of the coated tablets expressed as percent weight. The tablets were weighed, dried at 60 °C for 24 h and there weighed. %LOD was determined by the following equation:

$$\% LOD = \left[\frac{wtb - wta}{wtb} \right] \times 100$$

Optimized batch surface roughness was checked by Scanning Electronic Microscopy [24, 25].

In vitro drug release study

Drug release studies were carried out by using paddle type dissolution test apparatus (50 rpm, 37±0.5 °C) for 45 minute in purified water (900 ml). At the end of the time period, 10 ml of the samples were withdrawal and analyzed for drug content by using HPLC method at 195 nm [26, 27]

Optimization of aqueous coating process parameters by using 3² full factorial design

Two variables, spray rate and inlet air temperature were found critical. So, they were optimized using different trials, while other parameters were kept constant on the basis of previous coating study. On the basis of preliminary results, the coating spray rate (X_1) and the inlet air temperature (X_2) were chosen as independent variables in 3² full factorial design, while coating uniformity (CU), coating process efficiency (CPE), % loss on drying (%LOD) was

selected as dependent variables. Multiple linear regression analysis, ANOVA and graphical representation of the influence of factor by 3D plots were performed using of sigma plot software 11.0. The experimental runs and measured responses of 3² full factorial design batches of Aqueous Containing of GS-K tablets were depicted in table 4 [28-30].

Stability study of optimized batch

Optimized batch was packed in blister pack and was placed for stability study at 40°C/75% RH for 3 mo. Samples were evaluated after 3-month time for *in vitro* drug release study. The dissolution profile of product was compared using similarity factor, f_2 , which was calculated by following formula.

$$f_2 = 50 \log \left[\left\{ 1 + \frac{1}{n} \sum_{i=1}^n (R_i - T_i)^2 \right\}^{-0.5} \times 100 \right]$$

Where, \log is logarithm to the base 10, n is the number of time points, \sum is summation over all time points, R_t is the mean dissolution value of the reference profile at time t and T_t is the mean dissolution value of the test profile at the same time point. The USFDA draft guidance document contains more information on similarity factor (f_2). The value of similarity factor (f_2) between 50 and 100 suggests that the two dissolution profiles are similar [31, 32].

RESULTS AND DISCUSSION

Drug excipients compatibility study

The DSC thermograph of the GS-K (fig. 1), mixture (fig. 2) Correlated spectrum of drug and mixture (fig. 3) were obtained. The thermograph of pure GS-K showed a melting endothermic peak at 208.94 °C. The thermograph of excipients showed a melting endothermic peak at 209.25 °C. The DSC thermograms of the mixer showed sharp distinct endothermic peaks for Glucosamine sulfate potassium chloride and the excipients. This indicates that the drug did not interact with excipients [33].

Evaluation of glucosamine sulfate potassium chloride core tablet

Trial batch of GS-K core tablet showed angle of repose range from 23.51-27.58, carr's index range from 6.89-18.75 and hausner's ratio range from 1.07-1.19. All the tablets passed the weight variation test and it was found within the pharmacopoeia limits. Hardness of the tablets was found to be between 2.56-6.5 kg/cm². The thickness and friability of all the formulation was found to be in the range of 5.2 to 5.7 mm and 0.35 to 1.2, respectively. Disintegration time of all the formulation was found to be between 3.4 to 4.1 min was shown in table 2. The core tablets of Batch T1 and T2 failed in hardness and friability test. Batch T3 showed good hardness but disintegration time was high. Disintegration time was decreased in Batch T4 and T5 respectively. So, batch T5 was selected as a final core formulation [16-19].

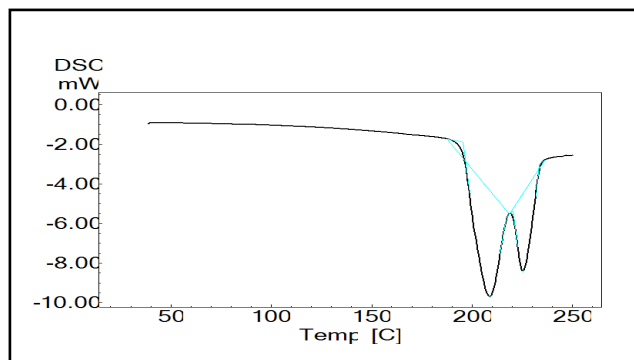


Fig. 1: DSC spectrum of glucosamine sulfate potassium chloride

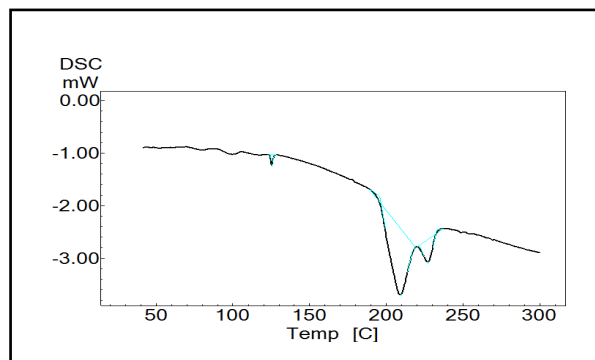


Fig. 2: DSC spectrum of the mixture

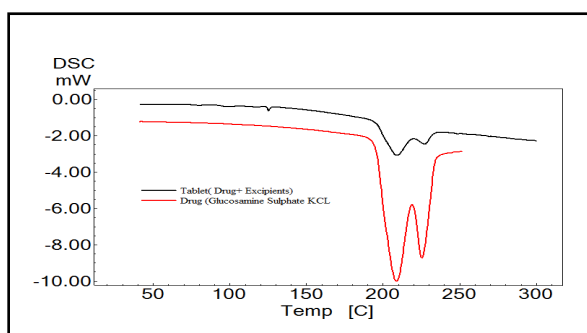


Fig. 3: DSC Co-related spectrum of drug and mixture

Table 2: Evaluation of glucosamine sulfate potassium chloride core tablet

Batch	T1	T2	T3	T4	T5
Avg. Weight (mg)	1100±5	1099±2	1099±4	1101±4	1100±3
Hardness (kg/cm ²)	2.56±0.2	4.90±0.3	6.2±0.4	6.4±0.4	6.5±0.6
Thickness (mm)	5.2±0.1	5.5±0.1	5.4±0.2	5.6±0.1	5.7±0.1
Friability (%)	1.2±0.3	0.85±0.1	0.48±0.4	0.42±0.3	0.35±0.2
Disintegration Time (min)	4.1±0.4	6.3±0.2	7.7±0.4	5.2±0.5	3.4±0.4

All values are expressed as mean±SD, n=3

Preliminary screening of coating parameters

Two variables, spray rate and inlet Air Temperature were found critical. So, they were optimized by using different trials, while other parameters were kept constant on the basis of previous coating study. Spray rate was adjusted 5, 7, 9, 11 and 13 gm/min and the batches were designated as B1 to B5 respectively. As shown in table 2 inlet air temperature was fixed at 50 °C. At a higher spray rate, sticking and picking were observed as compared to the lower spraying rates. At lower spray, rate coating efficiency was lower because the particles are dried between the paths before reaching to the tablet bed which also result in the rough surface. Batch B3 gave

good surface and highest coating process efficiency thus; it was decided to use 9 gm/min spray rate in further investigations. For batch B6 to B10 inlet air temperature was adjusted 30 °C, 40 °C, 50 °C, 60 °C and 70 °C respectively. As shown in table 3, Spray rate was fixed at 9 gm/min. At 30 °C sticking and picking were observed because the water was not evaporated from tablet surface and tablets stuck to each other. Nozzle block was observed when inlet air temperature was kept 70 °C, maybe because at the higher temperature, sprayed particles got dried very quickly. Hence, further trials were carried out using combination of inlet air temperature (45 °C to 55 °C) and spray rate (7 to 9 gm/min) in order to understand their effect and to optimize coating parameters [34, 35].

Table 3: Preliminary screening of coating parameters

Batch	Inlet air temperature (°C)	Spray rate (gm/min)	Coating uniformity (mg)	% Coating process efficiency	Surface roughness	%LOD	Conclusion
B1	50	5	2.1±0.03	72.58±1.2	4	0.42±0.2	+
B2	50	7	2.3±0.02	80.45±0.4	5	0.53±0.3	+
B3	50	9	1.8±0.04	86.62±0.8	6	0.76±0.5	+
B4	50	11	2.2±0.07	79.85±1.7	5	0.87±0.3	+
B5	50	13	-	-	-	-	Sticking and picking
B6	30	9	-	-	-	-	Sticking and picking
B7	40	9	2.4±0.06	79.63±1.4	6	0.96±0.5	+
B8	50	9	1.9±0.05	87.56±1.6	7	0.70±0.3	+
B9	60	9	2.1±0.05	81.35±0.6	5	0.56±0.2	+
B10	70	9	2.5±0.04	68.75±1.4	5	0.45±0.6	Nozzle block

All values are expressed as mean±SD, n=3

Table 4: Runs and measured responses of 3² factorial design of aqueous coating process parameters

Batch code	Spray rate (X ₁)	Inlet air temperature (X ₂)	Coating uniformity (Y ₁)	Coating process efficiency (Y ₂)	% Loss on drying (Y ₃)
F1	-1	-1	1.92	80.42	0.51
F2	0	-1	2.03	76.26	0.59
F3	1	-1	2.19	72.86	0.53
F4	-1	0	1.98	88.29	0.61
F5	0	0	2.12	86.45	0.7
F6	1	0	2.27	80.56	0.68
F7	-1	1	2.11	78.58	0.62
F8	0	1	2.28	73.65	0.71
F9	1	1	2.36	70.35	0.69
Factors and the levels in the design					
Independent variables			Low (-1)	Medium (0)	High (1)
Spray rate (X ₁)			7	9	11
Inlet air temperature (X ₂)			45	50	55

3² Full factorial design model evaluation

A statistical model incorporating interactive and polynomial terms was used to evaluate the responses:

$$Y = b_0 + b_1X_1 + b_2X_2 + b_{11}X_1^2 + b_{22}X_2^2 + b_{12}X_1X_2$$

Where, Y is the dependent variable, b₀ is the arithmetic mean response of the 9 runs and any b_i is the estimated coefficients for the related factor X_i. The main effects (X₁ and X₂) represent the average result of changing one factor at a time from its low to high value. The polynomial terms (X₁² and X₂²) are included to investigate nonlinearity. The interaction term "X₁X₂" shows how the response changes when the two factors change simultaneously. Evaluation data for core tablets and coated tablets were presented in table 5 and 6 respectively. The fitted equations relating the responses that is, coating uniformity (CU), coating process efficiency (CPE) and % loss on drying (%LOD) to the transformed factor are shown in table 4. The polynomial equations can be used to draw conclusions after considering the magnitude of coefficient and the mathematical sign it carries (i.e. positive or negative). The results of ANOVA suggested that F values calculated for CU, CPE and % LOD are 50.980, 55.714 and 84.632 respectively (table 7). Tabulated F value was found to be

9.013 at α = 0.05. Calculated F values are greater than tabulated for all dependent variables, therefore, factors selected have shown significant effects. From the results of multiple regression analysis, it was found that all factors had a statistically significant influence on all dependent variables as p < 0.05 (table 8) [36, 37].

Full and reduced model for coating uniformity

The coating uniformity for coated tablets was found to be varied from 1.92 to 2.36 and it showed a good correlation coefficient of 0.988. From the graph (fig. 4) and the regression coefficient values of factors, it was concluded that the spray rate gives more effect on coating uniformity as compared to inlet air temperature. For coating uniformity, the significance levels of the coefficients b₁₁, b₂₂, and b₁₂ were found to be P = 0.727, 0.804 and 0.268 respectively, so they were omitted from the full model to generate a reduced model. The P value for variable X₁ and X₂ were found 0.001 and 0.002 respectively (P < 0.05), which indicate that X₁ and X₂ both variable shown a significant effect on coating uniformity [36, 37]. Hence they were retained in the reduced model. The reduced model for coating uniformity:

$$CU = 2.127 + 0.135 X_1 + 0.102 X_2$$

Table 5: Evaluation of core tablets for factorial batches

Powder blend	Hardness (kg/cm ²)	Thickness (mm)	Friability (%)	Avg. wt. (mg)	Disintegration time (min)
F1	6.1±0.13	5.7±0.13	0.450±0.2	1100±0.9	3.2±0.5
F2	6.5±0.21	5.6±0.21	0.448±0.4	1101±0.7	3.3±0.8
F3	6.0±0.09	6.0±0.09	0.506±0.7	1098±1.1	3.3±0.4
F4	5.8±.32	5.8±.32	0.656±0.2	1100±1.2	3.4±0.6
F5	6.4±0.24	5.9±0.24	0.394±0.6	1100±0.9	3.4±0.4
F6	5.9±0.17	5.7±0.17	0.436±0.3	1102±1.1	3.5±0.6
F7	5.9±0.27	5.9±0.27	0.353±0.4	1102±0.9	3.5±0.8
F8	6.4±0.34	5.8±0.34	0.459±0.1	1100±0.8	3.2±0.6
F9	5.8±0.14	6.1±0.14	0.567±0.5	1101±1.2	3.4±0.4

All values are expressed as mean±SD, n=3

Table 6: Evaluation of coated tablets for factorial batches

Factorial batches	Hardness (kg/cm ²)	Thickness (mm)	Avg. wt. (mg)	Disintegration time (min)	% Drug release at 45 min
F1	6.7±0.13	6.3±0.10	1123±0.9	3.5±0.6	81.47±1.6
F2	7.1±0.21	6.1±0.13	1121±1.1	3.7±0.8	79.12±1.5
F3	6.9±0.09	6.4±0.12	1124±1.2	3.8±0.5	75.83±0.7
F4	6.8±0.32	6.1±0.06	1120±0.8	3.2±0.8	82.68±1.5
F5	7.0±0.24	6.5±0.02	1123±0.6	3.5±0.5	86.24±0.7
F6	6.9±0.17	6.1±0.14	1118±0.9	3.6±1.0	81.24±1.3
F7	7.3±0.27	5.8±0.06	1124±1.2	3.4±0.6	79.57±1.2
F8	7.1±0.34	6.2±0.04	1123±0.8	3.6±0.7	76.82±1.1
F9	6.9±0.14	6.4±0.07	1122±0.9	3.8±0.4	73.2±1.8

All values are expressed as mean±SD, n=3

Full and reduced model for coating process efficiency

Coating process efficiency of coated tablets was found to be varied from 70.35 to 88.29 and it's showed good correlation co-efficient of 0.989. For coating process efficiency, as seen from fig. 5, the 3D plot revealed that a corresponding increase spray rate, there were decreases in coating process efficiency and corresponding increase in inlet air temperature there also decreased the coating process efficiency. From regression, it is observed that only X_1 and X_2^2 were

significant model terms which affect the coating process efficiency. Interaction and nonlinearity was not observed. The P value for variable X_1 and X_2^2 were 0.003 and 0.001 ($P < 0.05$), which indicate that both variable has a significant effect on the coating process efficiency [36, 37]. Hence they were retained in the reduced model. The reduced model for Coating process efficiency:

$$CPE = 85.284 - 3.920 X_1 - 9.747 X_2^2$$

Table 7: Analysis of variance (ANOVA) of dependent variable

Source of variation	DF	SS	MS	F value	P Value
CU Dependent variable					
Regression	5	0.173	0.034		
Residual	3	0.002	0.0006	50.980	0.004
Total	8	0.175	0.021		
CPE Dependent variable					
Regression	5	290.532	58.106		
Residual	3	3.129	1.043	55.714	0.004
Total	8	293.661	36.708		
% LOD Dependent variable					
Regression	5	0.043	0.008		
Residual	3	0.0003	0.0001	84.632	0.002
Total	8	0.043	0.005		

Table 8: Summary of multiple regression analysis for coating process parameters

Responses	Model	Coefficient of regression parameters						R ²
		b ₀	b ₁	b ₂	b ₁₁	b ₂₂	b ₁₂	
coating uniformity	Full	2.127	0.135	0.102	-0.005	0.005	-0.025	0.988
	Reduced	2.127	0.135	0.102	-	-	-	-
coating process efficiency	Full	85.284	-3.920	-1.160	-0.167	0.277	-9.747	0.989
	Reduced	85.284	-3.920	-	-	-	-9.747	-
%Loss on drying	Full	0.703	0.0267	0.065	0.012	0.060	0.055	0.993
	Reduced	0.703	0.0267	0.065	-	0.060	0.055	-

Full and reduced model for % loss on drying

The % LOD of coated tablets was found to be varied from 0.51 to 0.71 and showed good correlation co-efficient of 0.993. For % LOD, as seen from fig. 6, the 3D plot revealed that a corresponding increase in spray rate, there was increase in % Loss on drying and the corresponding increase in inlet air temperature there was also increase in the % loss on drying. From regression, it is observed that X_1 , X_2 , X_1^2 and X_2^2 were significant model terms which affect the % loss on drying. Interaction and nonlinearity were not observed. The P value for variable X_1 , X_2 , X_1^2 and X_2^2 were 0.008, 0.001, 0.004 and 0.005 respectively [36, 37]. Hence they were retained in the reduced model. The reduced model for %Loss on drying

$$\% \text{ LOD} = 0.703 + 0.0267 X_1 + 0.0650 X_2 - 0.0600 X_1^2 - 0.0550 X_2^2$$

Validation of the design

To validate the evolved mathematical models (reduced models) one checkpoint was selected as shown in table 9. Good correlation was found between observed and predicted values as shown in table 10.

Hence, it was concluded that the evolved models may be used for theoretical prediction of responses within the factor space [36, 37].

Selection of optimized batch in factorial design study

Drug release of all batches was carried out for 45 min. It was observed that (as shown in table no 5) maximum drug release was found in batch F5 and other all batches gave less drug release as compared to batch F5. Hence, batch F5 was selected as an optimized batch. The optimized formulation was subjected to SEM and accelerated stability study.

Stability study of optimized batch

Short term accelerated stability study showed that there was no significant change in the formulation after 3 mo and the evaluation result was found within the limit. The results are shown in table 11. Batch F₅ was kept for the stability study. The *in vitro* release profile at initial and after 3 mo was compared using similarity factor, f_2 , value which was found to be 88.50. There is no significant difference in similarity factor, f_2 , value which indicated that the prepared formulation was stable [38].

Table 9: Formulation of checkpoint batches

Batch code	Variable level			
	Coded value		Actual value	
	X_1	X_2	X_1 (mg)	X_2 (ml)
CP1	-0.5	-0.5	8	47.5

Table 10: Evaluation of checkpoint batches and comparison with predicted value

Parameter	Actual value	Predicted value
coating uniformity	2.1	2.008
coating process efficiency	79.23	78.450
% loss on drying	0.721	0.714

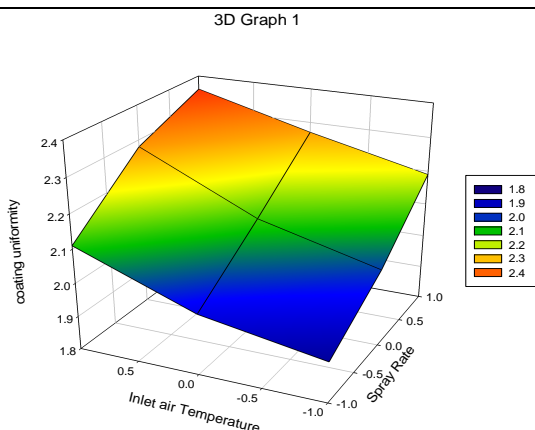


Fig. 4: Effect of spray rate (X_1) inlet air temperature (X_2) on coating uniformity

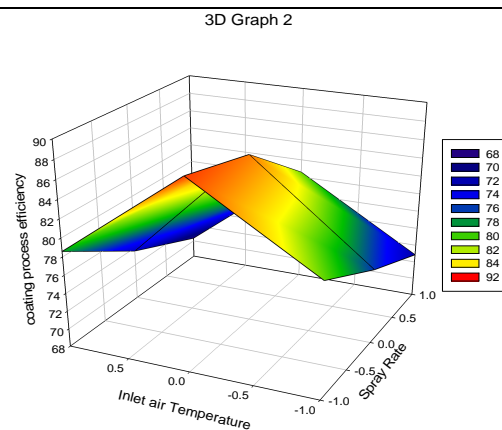


Fig. 5: Effect of spray rate (X_1) inlet air temperature (X_2) on coating process efficiency.

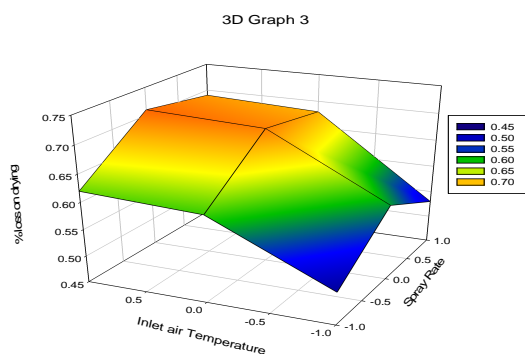


Fig. 6: Effect of spray rate (X_1) inlet air temperature (X_2) on % loss on drying.

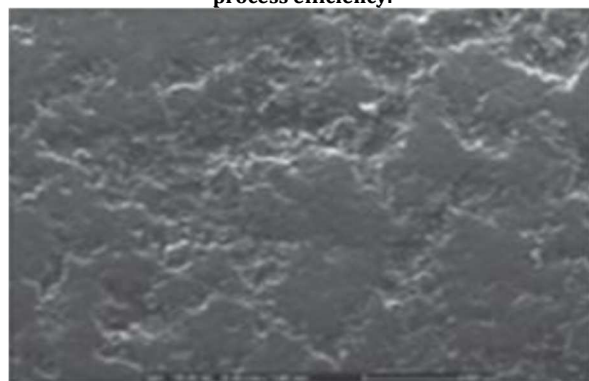


Fig. 7: SEM of coated tablet surface

Table 11: Comparative study of optimized batch with market product

S. No.	Parameters	Initial (Batch F5)	After 3 mo (Batch F5)
1	Hardness (kg/cm ²)	7.0±0.21	6.8±0.14
2	Average weight (mg)	1123±1.3	1121±0.7
3	Disintegration time (min)	3.5±0.3	3.4±0.4
4	Assay	99.50±0.4 %w/w	98.90±0.5 %w/w
5	<i>In vitro</i> drug release (After 45 min.)	86.24±1.5	83.70±1.5

All values are expressed as mean±SD, n=3

CONCLUSION

In this study, an aqueous-based film coating process of glucosamine sulfate potassium chloride tablets was performed in a side-vented perforated pan coating apparatus (auto coater). The preliminary results revealed that spray rate, and inlet air temperature had a major effect on tablet coating performances. The spray rate of coating solution 9 gm/min and inlet air temperature 50 °C considered as an optimum aqueous film coating of special shaped tablets in auto coater coating machine. An optimized batch was found stable. It showed that aqueous based film coating process is compatible with the drug. Moreover, the process of film coating in developed formulation is eco-friendly, non-hazardous and cost-effective.

AUTHORS CONTRIBUTIONS

All the author have contributed equally

CONFLICT OF INTERESTS

Declared none

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